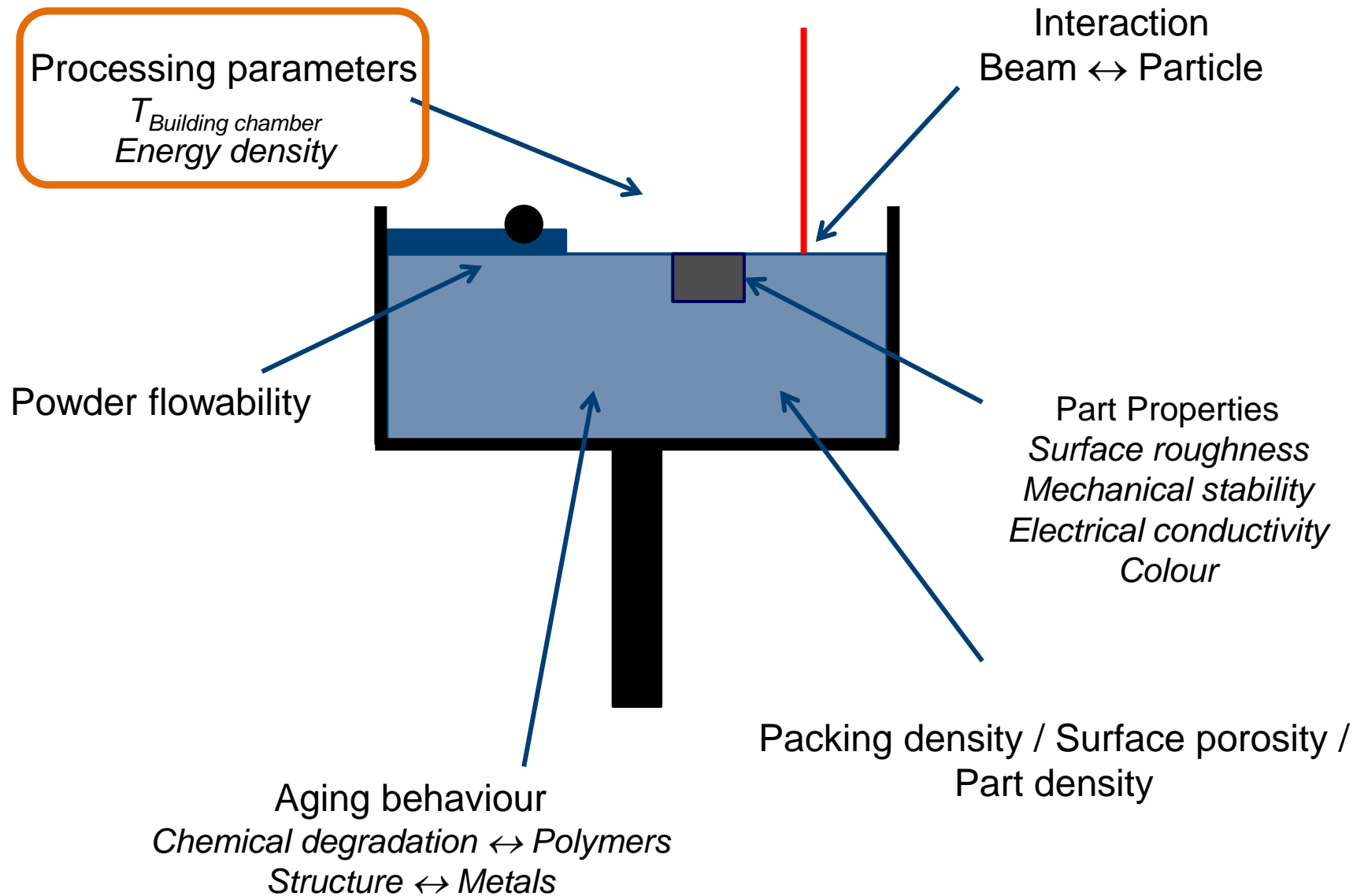


Tailoring the melting behaviour of LBM powders

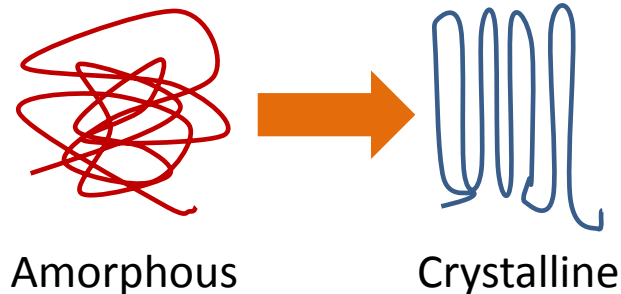
Marius Sachs, Jochen Schmidt, Stephanie Fanselow and
Karl-Ernst Wirth

University of Erlangen - Nuremberg



- Overcome material limitations in LBM processes
 - Processing of multi-materials
 - Not possible due to different preheating temperatures of the building chamber
 - Adjustment of this preheating temperature possible by changing crystalline state of polymeric material

→ Increase of crystalline structure

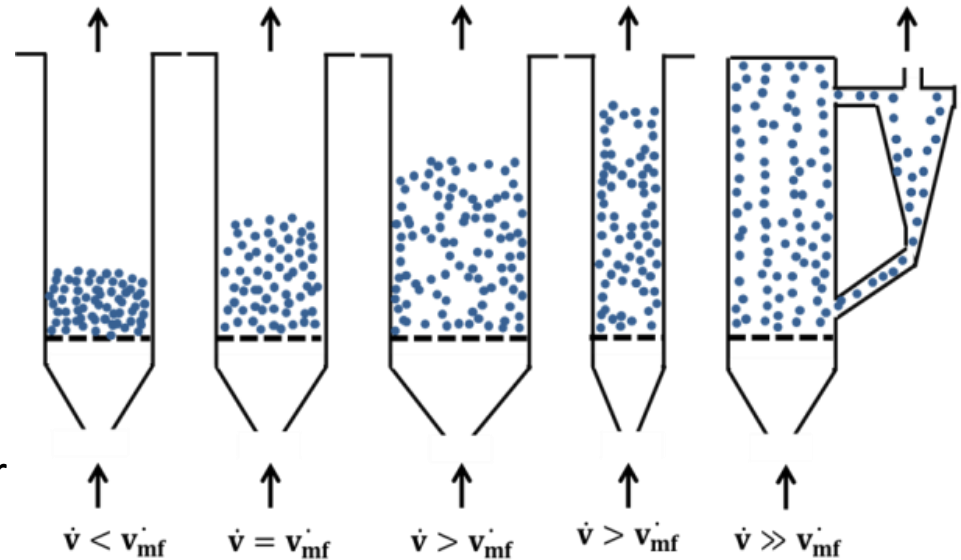


- Process route
 - Manipulation of crystalline structure of polymeric material
 - Possible by heat treatment
 - Temperature just below melting temperature

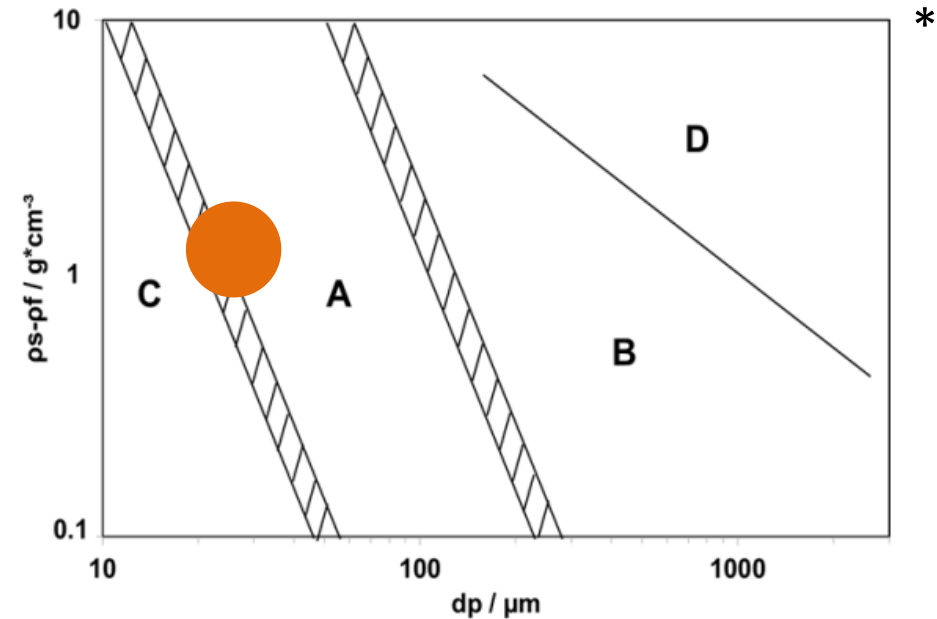
- Prerequisite
 - Temperature adjustable within few °C
 - No temperature gradients
 - Scale-Up to industrial range

→ Fluidized Bed Reactor

- Powder bulk flow through by gas
- Gas velocity exceeds gravity force
 - Particles show liquid behaviour
 - Excellent heat and mass transfer
 - No “hot spots” due to temperature gradients

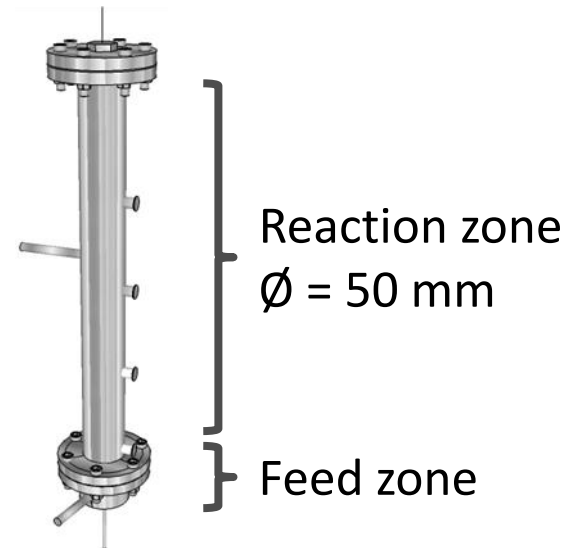


- A (aeratable)
 - Small particle size & small density
→ Good fluidization behavior
- B (bubbling)
 - Increased particle size
→ Formation of gas bubbles
- C (cohesive)
 - Small particle size & low density
→ Bad flowability and fluidization
- D (dense)
 - High density and rather big particles
→ Poor fluidization behavior

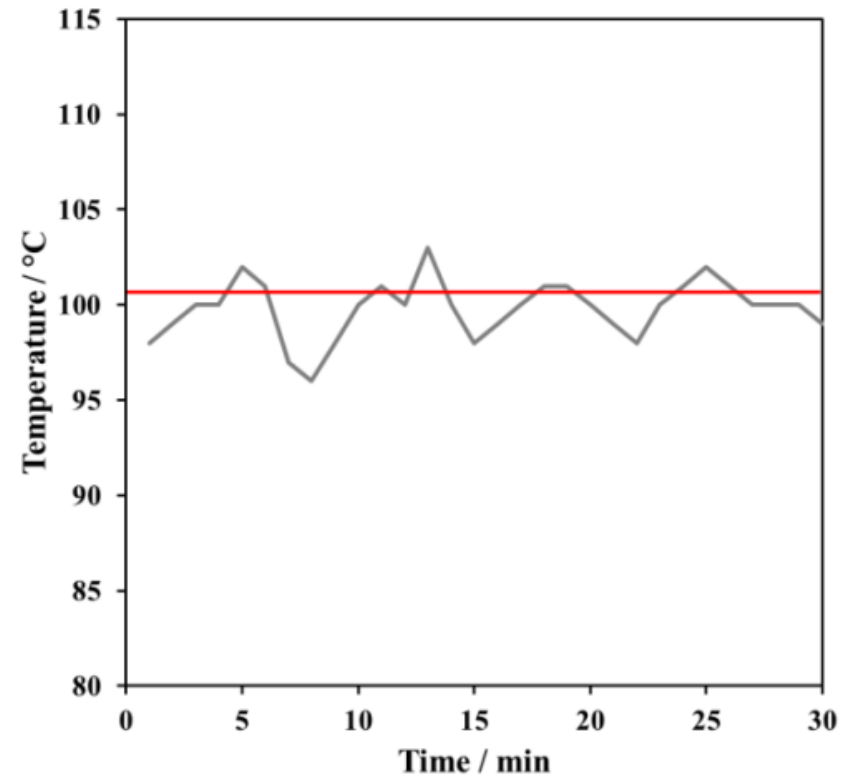


* D. Geldart: "Types of gas fluidisation"; Powder Technology, Volume 78, Issue 5, 1973

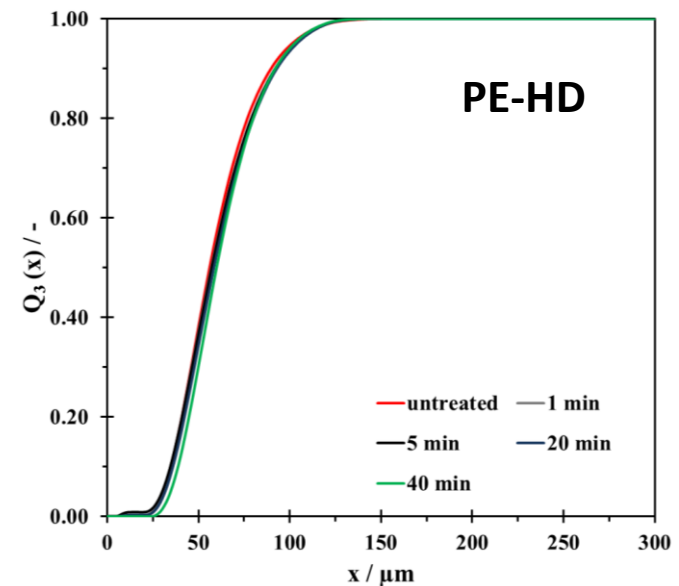
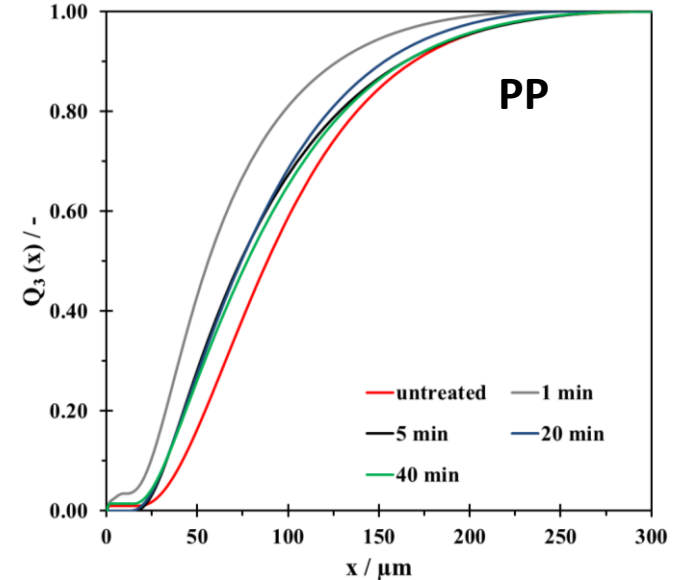
- Reactor
 - Fluidized Bed Reactor
 - Diameter 50 mm
 - Lab scale for proof-of-concept
 - Material: Stainless steel
 - Fluidization gas N₂
 - No oxidative degradation
- Material
 - Polyethylene-HD
 - Coathylene NB5374, DuPont CH
 - Polypropylene
 - Coathylene PD 0580, DuPont CH
 - Powder material coated with nanoscale fumed silica
 - Improved flowability



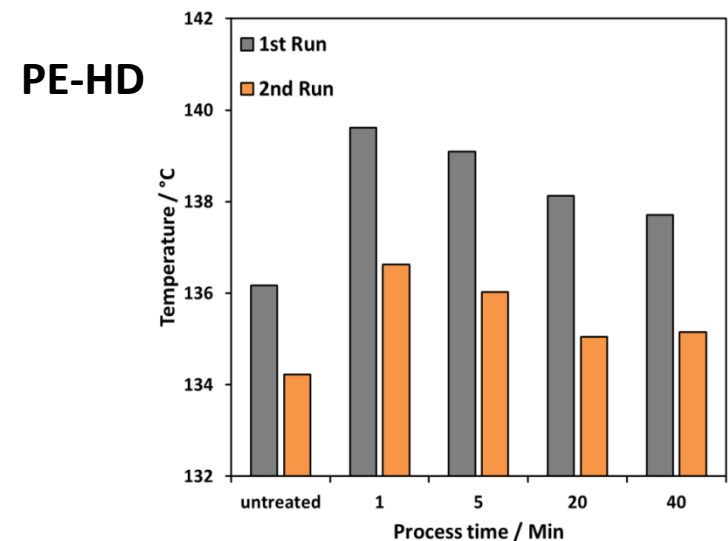
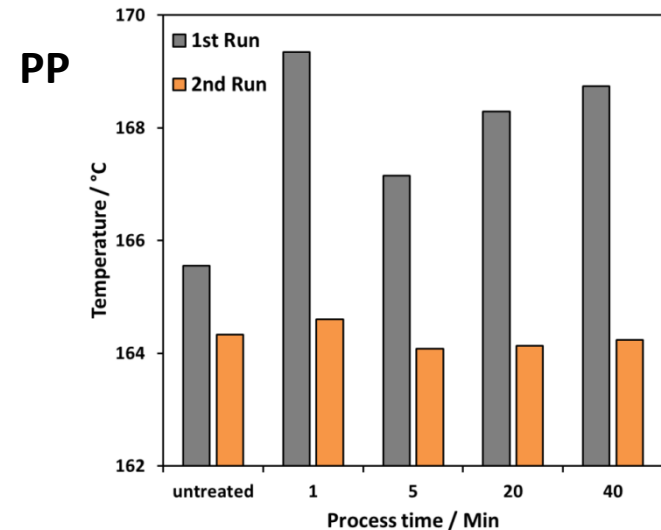
- Temperature necessary close to T_{Melting}
- Inaccuracy / Fluctuation of T_{Reactor} to be avoided
 - Otherwise: Melting of polymer powders
 - Reactor concept gives opportunity to set the reactor temperature within few °C
- Heating time to treatment temperature
 - Set-to 15 Min



- Particle size distribution measured by Malvern Mastersizer
 - No major shifts observable
 - Melting of polymer material is avoided within treatment procedure
 - Coating of fumed silica not affected by treatment
 - Observed using SEM
- No effect of heat treatment on flowability and thus behaviour of material in deposition process



- Maximum increase of peak temperature after 1 min treatment time
- Effect of increasing treatment time
 - Polypropylene
 - No degradation effects observable
 - Crystallisation further increases
 - Polyethylene
 - Degradation effects due to longer treatment times
- Effects in 2nd heating procedure
 - Polypropylene
 - No degradation observable
 - Polyethylene
 - Again decrease measured
 - Degradation of polymeric structure



- Increase of melting enthalpies after 1 min treatment time in FBR

- Fast kinetics of structural change

- Polypropylene

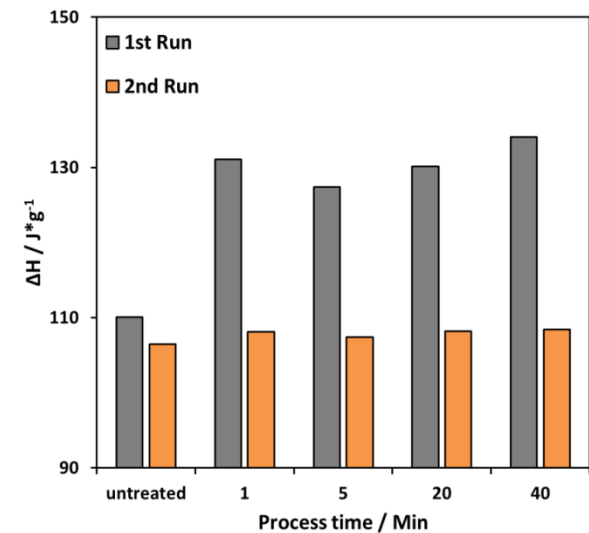
- No effect with increasing treatment time
 - Crystalline state does not further increase

- Polyethylene

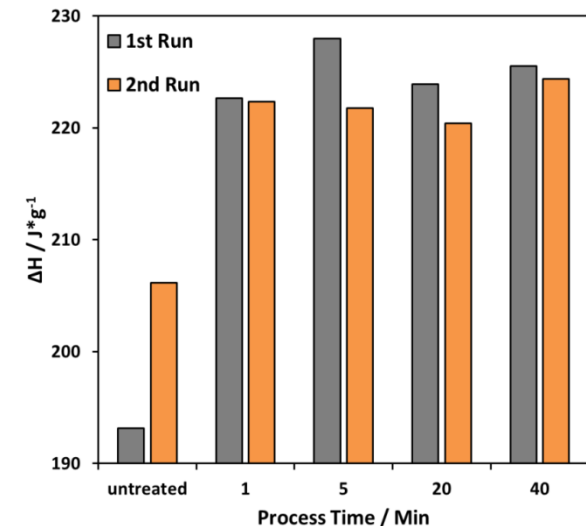
- Further change of necessary melting heat
 - Degradation of polymeric structure

- Effect in 2nd heating procedure follow same principles

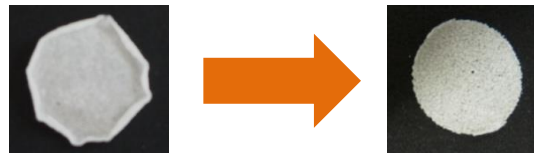
PP



PE-HD



- Treatment of sensitive polymer material near of melting temperature in fluidized bed reactor established
 - Control of process temperature within few °C possible
- Effect of heat treatment on thermal behaviour of material determined using Differential Scanning Calorimetry
 - Measured peak temperature and onset temperature controllable
 - Necessary melting enthalpies adjustable
- Manufacturing of single layers in LBM process (Cooperation with blz)
 - Dramatic reduction of curling effects due to thermal tensions
 - Increased stability of the material towards temperature fluctuations

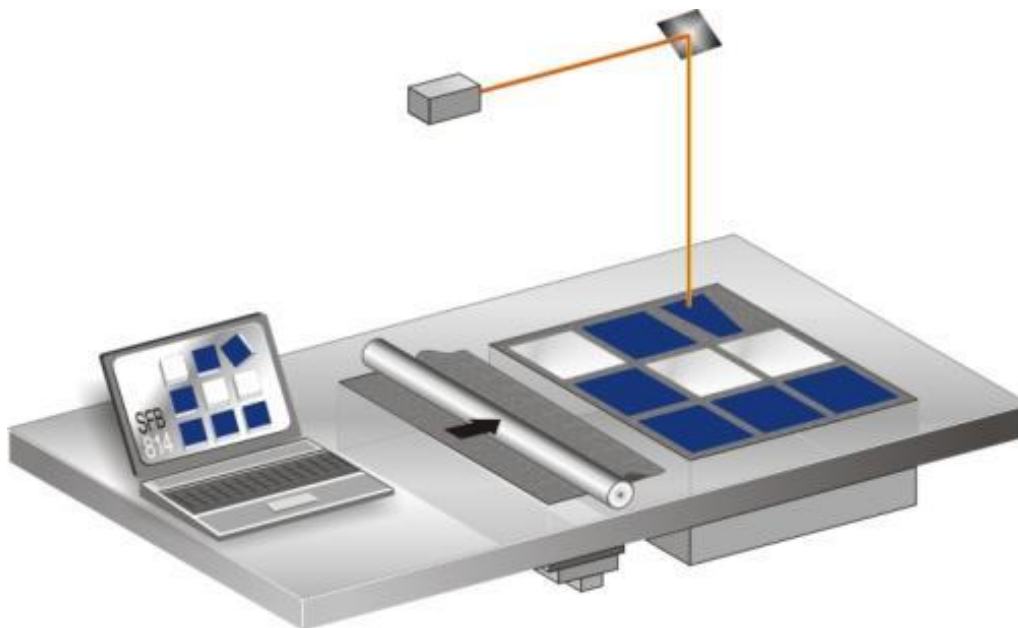


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Thank you for your attention!